

### **Amendments to the Claims:**

*This listing of claims will replace all prior versions, and listings, of claims in the application:*

1.(Currently Amended) A process for the recovery of nickel and/or cobalt from an impure nickel, cobalt or mixed nickel/cobalt material including the steps of:

a) providing a nickel, cobalt or mixed nickel/cobalt material ; and

b) contacting the nickel, cobalt or mixed nickel/cobalt material with a feed ammoniacal ammonium carbonate solution and a reductant in a leach step, wherein the reductant is selected from a mixed cobalt/nickel sulphide, cobalt sulphide or nickel sulphide.

2. (Original) A process according to claim 1, wherein the nickel, cobalt or mixed nickel/cobalt material is either a nickel, cobalt or mixed nickel/cobalt hydroxide, carbonate, basic carbonate or basic sulphate material.

3. (Previously Presented) A process according to claim 1, wherein the nickel, cobalt or mixed nickel/cobalt material is a mixed nickel/cobalt hydroxide material.

4. (Previously Presented) A process according to claim 1, wherein the feed ammoniacal ammonium carbonate solution is a process liquor from a Caron type process.

5. (Cancelled).

6. (Currently Amended) A process according to claim-~~5~~ 1, wherein the reductant is a mixed cobalt/nickel sulphide and is produced by contacting a cobalt/nickel containing ammoniacal ammonium carbonate solution with ammonium hydrosulphide or sodium hydrosulphide, to precipitate a mixed cobalt/nickel sulphide.

7. (Cancelled).

8. (Currently Amended) A process according to claim ~~7~~ 6, wherein the cobalt/nickel containing ammoniacal ammonium carbonate solution is a portion of the process liquor of a Caron type process used as the feed ammoniacal ammonium carbonate solution, or a portion of any selected cobalt/nickel containing process liquor.

9. (Cancelled).

10. (Previously Presented) A process according to claim 1 wherein the feed ammoniacal ammonium carbonate solution and the cobalt/nickel containing ammoniacal ammonium carbonate solution contain 8 to 16% by wt ammonia, 4 to 12% by wt carbon dioxide, 0.5 to 1.5% by wt nickel and 0.02 to 0.2% by wt cobalt.

11. (Currently Amended) A process according to claim 1 wherein the mixture of the nickel, cobalt or mixed nickel/cobalt material, the feed ammoniacal ammonium carbonate solution and reductant is agitated for a period of from 30 minutes to 12 hours at a temperature of from 30 to 90°C at atmospheric or elevated pressure.

12. (Cancelled).

13. (Currently Amended) A process according to claim ~~12~~ 11 wherein air or oxygen containing gas is injected into the mixture after a period of at least 10 minutes anaerobic agitation.

14. (Currently Amended) A process ~~for the recovery of nickel and/or cobalt from a nickel, cobalt or mixed nickel/cobalt material including the steps of~~ according to claim 1, wherein the leach step includes:

~~a) providing a nickel, cobalt or mixed nickel/cobalt material;~~

~~b) a) a primary leach step wherein~~ a) a primary leach step wherein ~~contacting the nickel, cobalt or mixed nickel/cobalt material is contacted~~ contacted with a feed ammoniacal ammonium carbonate solution

to produce a product solution ~~containing the majority of the nickel and cobalt~~ and a residue;

~~e) b)~~ separating the residue from the product solution; and

~~d) c)~~ a secondary leach step wherein the residue is contacted with fresh ammoniacal ammonium carbonate solution and a reductant ~~in a secondary leach step to produce a secondary product solution containing the dissolved nickel and cobalt and a secondary leach residue;~~

wherein the reductant is selected from a mixed nickel/cobalt hydroxide, cobalt sulphide or nickel sulphide.

15. (Original) A process according to claim 14, wherein the nickel, cobalt or mixed nickel/cobalt material is either a nickel, cobalt or mixed nickel/cobalt hydroxide, carbonate, basic carbonate or basic sulphate material.

16. (Previously Presented) A process according to claim 14, wherein the material is a mixed nickel/cobalt hydroxide material.

17. (Original) A process according to claim 14 wherein the feed ammoniacal ammonium carbonate solution is a process liquor from a Caron type process.

18. (Original) A process according to claim 14 wherein the secondary product solution is returned and combined with the feed ammoniacal ammonium carbonate solution for the primary leach step.

19. (Original) A process according to claim 14 including the further step wherein the secondary leach residue is subjected to a third leach step by subjecting the secondary leach residue to prolonged contact with a strong ammoniacal ammonium carbonate solution.

20. (Original) A process according to claim 19, the strong ammoniacal ammonium carbonate solution contains 8 to 16 wt% ammonia, 4 to 12 wt% carbon dioxide, 0 to 1.0 wt% nickel, and 0 to 0.1 wt% cobalt.

21. (Cancelled).

22. (Currently Amended) A process according to claim ~~21~~ 14 wherein the reductant is a mixed cobalt/nickel sulphide and is produced by contacting a cobalt/nickel containing ammoniacal ammonium carbonate solution with ammonium hydrosulphide or sodium hydrosulphide to precipitate a mixed cobalt/nickel sulphide.

23. (Cancelled).

24. (Currently Amended) A process according to claim ~~23~~ 22, wherein the cobalt/nickel containing ammoniacal ammonium carbonate solution is a portion of the process liquor of a Caron type process used as the feed ammoniacal ammonium carbonate solution, or a portion of any selected cobalt/nickel containing process liquor.

25. (Previously Presented) A process according to claim 14 wherein the feed ammoniacal ammonium carbonate solution and the cobalt/nickel containing ammoniacal ammonium carbonate solution contains 8 to 16% by wt ammonia, 4 to 12% by wt carbon dioxide, 0.5 to 1.5% by wt nickel and 0.02 to 0.2% by wt cobalt.

26. (Original) A process according to claim 14 wherein the fresh ammoniacal ammonium carbonate leach solution for the secondary leach step contains from 8 to 16% by wt ammonia and 4 to 12% by wt carbon dioxide with only trace amounts of nickel and cobalt.

27. (Currently Amended) A process according to claim 14 wherein the mixture of the fresh ammoniacal ammonium carbonate leach solution, the residue of the primary leach step and the reductant is agitated for a period of from 30 minutes to 12 hours at a temperature of from 30 to 90°C at atmospheric or elevated pressure.

28. (Cancelled).

29. (Currently Amended) A process according to claim ~~28~~ 27 wherein air or oxygen containing gas is injected into the mixture after a period of at least 10 minutes anaerobic agitation.

30-32. (Cancelled).